

SUBMITTAL TRANSMITAL

September 10, 2012 WCM Submittal No: 11377-001

- PROJECT: Harold Thompson Regional WRF Birdsall Rd. Fountain, CO 80817 Job No. 2908
- ENGINEER: GMS, Inc. 611 No. Weber St., #300 Colorado Springs, CO 80903 719-475-2935 Roger Sams
- OWNER: Lower Fountain Metropolitan Sewage Disposal District 901 S. Santa Fe Ave. Fountain, CO 80817 719-382-5303 James Heckman
- CONTRACTOR: **Tideflex Technologies** 600 N. Bell Ave. Carnegie, PA 51066 Jeff Kelly jkelly@redvalve.com

SUBJECT: Submittal for Coarse Bubble Diffuser Systems for Aerobic Digesters No. 1, 2 & 3 Requesting Review Response by 9/19/12.

SPEC SECTION: 11377

PREVIOUS SUBMISSION DATES:

DEVIATIONS FROM SPEC: ____ YES X__ NO

CONTRACTOR'S STAMP: This submittal has been reviewed by Weaver Construction Management and, unless indicated otherwise, has been found to be in conformance with the intent of the contract documents.

Contractor's Stamp:	Engineer's Stamp:
Date: 9/10/12 Reviewed by: John Jacob () Reviewed Without Comments (X) Reviewed With Comments	
ENGINEER'S COMMENTS:	



CERTIFICATE OF CONFORMANCE

Company:	Weaver Construct. Mgmnt.	Date:	09/07/2012
P.O. No.:	9103-11377	S.O. No.:	OP# 10372

This is to certify that all products manufactured by Red Valve Company, Tideflex Technologies¹ or RKL Controls¹ for this order and referenced below, [X] will be [] were manufactured² in the USA, and in compliance with the requirements of the above referenced Purchase Order and the applicable codes, standards and specifications referenced therein.

S.O.			
No.	Part Number	Description	Qty.
	undetermined	Coarse Bubble Aeration Systems	3
		For Aerobic Digesters No.1, No.2, No.3	

Project/Job: Harold D. Thompson Regional Water Reclamation Facility

² Manufacturing facilities are located in Carnegie, Pennsylvania, USA, and Gastonia, North Carolina, USA.

Approved By:

T. Pull Jeffrey T. Kelly

Aeration Systems Product Manager

Date:

September 7, 2012

This Certificate of Conformance is prepared in good faith and is limited to those plans and specifications received. Red Valve Company, Inc. does not assume responsibility for any other codes, standards or specification sections if not submitted or received at the time of quotation or order.

¹ A division of Red Valve Company, Inc.

INSTALLATION PLANS TIDEFLEX DIFFUSED AERATION SYSTEM



DRAWING No.	SHEET No.	SYSTEM DRAWINGS
AS12-10372	1 OF 5	DIFFUSED AERATION SYSTEM – TITLE SHEET
AS12-10372	2 OF 5	AERATION SYSTEM – ASSEMBLY PLAN
AS12-10372	3 OF 5	AERATION SYSTEM – SECTION VIEW "A-A"
AS12-10372	4 OF 5	AERATION SYSTEM – SECTION VIEW "B-B"
AS12-10372	5 OF 5	PIPE SUPPORT LOCATIONS AND INFO
		APPENDIX DRAWINGS
A-103.01.010	1 OF 1	DROP PIPE WALL BRACKET – INSTALLATION DETAILS
A-104.00.010	1 OF 1	HORIZONTAL PIPE SUPPORT ASSEMBLY - INSTALLATION PROCEDURES
A-104.02.011	1 OF 2	COARSE BUBBLE DIFFUSER AND SADDLE ASSEMBLY SECTIONS
A-104.02.011	2 OF 2	COARSE BUBBLE DIFFUSER AND SADDLE ASSEMBLY SECTIONS
A-104.06.020	1 OF 1	HORIZONTAL PIPE SUPPORT ASSEMBLY – BASE EXTENSION TYPE
A-104.07.011	1 OF 1	HORIZONTAL PIPE SUPPORT STABILIZER BAR DETAILS
A-107.01.010	1 OF 1	EXPANSION JOINT INSTALLATION PROCEDURES







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	SUPPO	RT DESIGI	NATIONS		NOMINAL PIPE SIZE	PIPE SIZE O.D.	ROD DIA.	NEOPRENE STRIP LENGTH	PART NUMBER	DO NOT OVER TIGHTEN RISER CLAMPS
	SHOW	IN ON PLA	AN AND	1	2"	2.375"	0.625"	7.00"	RUBBER-02-020X1/8	OUT OF ROUND BY OVER TIGHTENING OF PIPE SUPPORTS
	ELEVA	ATION SHE	ETS		2.5"	2.875"	0.625"	8.25"	RUBBER-02-020X1/8	
					3"	3.50"	0.625"	10.50"	RUBBER-02-020X1/8	1/16" CLEARANCE PROVIDED BETWEEN OUTSIDE
) denot	es rod len	igth "C" ri	EQUIRED	4"	4.50"	0.625"	13.75"	RUBBER-02-020X1/8	OF PIPE AND INSIDE OF RISER CLAMPS TO ALLOW
	/				6"	6.625"	0.625"	20.50"	RUBBER-02-020X1/8	FOR INSTALLATION OF 1/8" THICK NEOPRENE STRIP
					8"	8.625"	0.75"	26.75"	RUBBER-02-020X1/8	
	R DENO	TES LOCATIO	N		10"	10,750"	0.75"	33.25"	RUBBER-02-020X1/8	
\	PLATE				12"	12 750"	0.75"	39.75"	RUBBER-02-020X1/8	
					14"	14.00"	0.75"	43 75"	RUBBER-02-020X1/8	
	\						0.75	10.70		
	> DENOT	es pier hei	ight "h" Ri	EQUIRED	REFERENCE LETTER	DESCF	RIPTION	PART NUME VALUE	BER DEFINITION	
					A	MATE	RIAL			
S	DENO	TES LOCATIO	N					40	304 STAINLESS STEEL	
	FOR	STABALIZER	BAR					41	316 STAINLESS STEEL	
					В	PIPE DI	AMETER			
								020	2"ø	
								025	2.5"ø	
								0.30	.3"ø	
								040	4"ø	
								060		
								080	8"ø	
								100	10"ø	
								120	10 0	
								140	12.0	
								140		FOR 5/8"Ø R
							OD SDACING			L (DRILL 3/4"Ø
					U		OD SPACING	020	£ 00"	
								020	6.00"	FOR 3/4"Ø R
								025	6.00"	(DRILL 7/8"ø
								0.00	7.00"	
								040	7.00	(ADHESIVE AP
						<u> </u>		000	9.00	
						<u> </u>		100	14.00"	
						<u> </u>		100	14.00	* FOR SS DROP-IN ANCHORS (IN LIFU
						<u> </u>		140	10.00	MANUAL APPENDIX FOR RECOMMENDED C
						<u> </u>		140	10.00]
									THE DESIGN INFORMATION WITHIN T OCUMENTS IS THE INTELLECTUAL PROF	HESE S.O.#: QUOTE #: 10372
								F	RED VALVE COMPANY/TIDEFLEX TECHNO	DLOGIES. DWG. NOTES:
								co	ONSTRUCT DUPLICATE SYSTEMS; USE (JF THESE
								DO	CUMENTS AND/OR CONSTRUCTION OF SYSTEMS SHALL VIOLATE THE COPYRIG	DUPLICATE HT AND
								PA	ATENT PROTECTION LAWS ASSOCIATED	WITH THIS S SHALL
	1							'	REMAIN THE PROPERTY OF RED V	
									DISTRIBUTED FOR THE SOLE PURPOS	IV ARE SE_OF
A	JTK	09/06/12			ISSUE FOR APP	'ROVAL		S1	Coordinating the installation of (Stem(s) provided by RFD valve co	THE MPANY /
REV	BY	DATE	ECO#	CHK'D		DESCRIPTIC	DN		TIDEFLEX TECHNOLOGIES.	······································







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PIPE SUPPORT STABILIZER BARS FIELD INSTALLATION



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PIPE SIZE O.D.	SS RIGID VICTAULIC COUPLING PART NUMBER	ALLOWABLE PIPE SEP. "t"	BOLT TORQUE FT-LBS
2.375"	3750-41-VCP-RIG020	0.05"	18–27
2.875"	3750-41-VCP-RIG025	0.05"	18–27
3.50"	3750-41-VCP-RIG030	0.05"	45-50
4.50"	3750-41-VCP-RIG040	0.19"	45-50
5.00"	3750-41-VCP-RIG050	0.25"	75-100
6.625"	3750-41-VCP-RIG060	0.25"	125-200
8.625"	3750-41-VCP-RIG080	0.25"	200-300
10.75"	3750-41-VCP-RIG100	0.25"	200-300



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CLOSURE T TOOLS PROVIDED TOOLS CAN

PIPE SIZE O.D.	SS FXE VICTAULIC COUPLING PART NUMBER
2.375"	3750-41-VCOUPL020
2.875"	3750-41-VCOUPL025
3.50"	3750-41-VCOUPL030
4.50"	3750-41-VCOUPL040
6.625"	3750-41-VCOUPL060
8.625"	3750-41-VCOUPL080
10.75"	3750-41-VCOUPL100
12.00"	3750-41-VCOUPL120
14.00"	3750-41-VCOUPL140

TABLE GLOSSARY

L - DISTANCE FROM END OF PIPE TO NEAR EDGE OF END RING.

R - DIAMETER OF END RING.

DIM "G" DIM "C/E" DIM "W" 1.125" 0.125" 0.375" 0.75" 1.75" 0.188" 0.375" 1.25" 0.25" 0.625" 1.75"

: 1	00L	REG	UIRED	FOR	INS	TALLAT	ION	OF	COU	PLING	
DEI	DΒ	í tid	EFLEX	WILL	ΒE	INVOIC	ED	UNL	ESS	RETUR	RNED
Ν	ΒE	PURC	CHASED) FRO	ΜV	ICTAUL	.IC [DEPE	END-	0-LOP	(
8	00-	841-	-6624	ATLAN	ITA,	GEOR	GIA,	USA	4		

C/E





Tideflex[®] Diffused Aeration Systems

APPENDIX B – DESIGN CALCULATIONS

Diffused Aeration System Modeling Program

Harold D. Thompson Regional Water Reclamation Facility Aerobic Digesters No. 1,2,3 - Coarse Bubble Aeration & Mixing Systems

1.8% Solids - O2 & Mixing

Facility: Location: Contact: Email:	Harold D. Thompson Regional Water Reclamation Facility Fountain, Colorado Lower Fountain Metropolitan Sewage Disposal District
Consulting Firm:	GMS, Inc.
Location:	Colorado Springs, CO
Contact:	Mark Morton
Email:	mamorton@gmsengr.com
Fideflex Representative:	ICS Sales, Inc.
Location:	Westminister, CO
Contact:	Ted Whitfield
Revision Date:	9/5/2012 12:23
Revision Description:	Revision 3 - Final Design



Carnegie, PA 15106

info@tideflex.com

PHONE (412) 279-0044 FAX (412) 279-5410

Harold D. Thompson Regional Water Reclamation Facility Aerobic Digesters No. 1,2,3 - Coarse Bubble Aeration & Mixing Systems Input Data & Design Parameters for Biological / Chemical Process Systems Influent / Effluent Concentrations 0.0 0.00 0.0 Design COD effluent concentration 0.0 1.8% Solids - O2 & Mixing 0.0 0.0 0.0 Design NH4 effluent concentration **Owner / Engineer Provided Design Values** Pre-Determined AOR Value to be Applied 1.594.2 lbs/day 723.1 kg/day Oxygen Uptake Rate satisfied at design airflow rate 11.872 mg/l/hr **Process Design Values** 0 499 Lbs of Oxygen Required per lb. Of NH3 removed 4.30 MLSS Concentration for Activated Sludge Process 0 Food to BioMass ratio F/M 0.20 Sludge Process Solids Concentration 1.80 % Solids **Oxygen Transfer Efficiency Values** Diffuser distance from bottom of tank 0.25 0.1 m 10.3 3.1 Diffuser Depth (Dp) ft. m 5,413.0 1,649.9 Site Elevation above Mean Sea Level ft. m Barometric Pressure at Site (Pa) 24.19 in Hg 11.88 psia 81.930 kPa 14.70 Barometric Pressure at Mean Sea Level (Pmsl) 29.92 in Ha psia 101.320 kPa Process Water Salinity 0.00 ppt Surface Oxygen Saturation at 20 C (Cs) 9.09 mg/l Surface Oxygen Saturation at Temp (Cst) 8.58 mg/l Residual Dissolved Oxygen Level (DO) 2.00 mg/l Waste Water Temperature (T) 73.4 23.0 Diffuser Variables Coarse Bubble **Fine Bubble** Model Number TFX-40 **TFA-3.00** @ 1.8% Solids Alpha Factor 0.35 Alpha Factor 0.45 Beta Factor 0.950 Beta Factor 0.950 Disclaimer: The calculations, projections and Theta Factor 1.024 Theta Factor 1.024 values produced within this model are based upon the applied site specific values as shown on the Depth Correction Factor (f) 0.40 0.25 Input Data page and any other related pages. Corrected Saturation at Std. for Depth (Css) 10.19 9.78 mg/l mg/l These site specific values may have been provided Corrected Saturation at Temp. for Depth (Csw) 7.98 ma/l 7.59 mg/l by the facility owner, consulting engineer or derived Blower Parameters from industry standards. Any variance in these values will effect the projections produced within 37.7 Inlet Blower Air Temperature at the Site 100 С this model. This model is intended to provide Saturated Vapor Pressure at Site Temperature 0.9503 psia 6.552 kPa design guidance related to the operation of the Relative Humidity at the Site 50% Tideflex System and/or Tideflex components. Air 70% Diffuser data applied within the model is derived Applied Blower Efficiency from certified performance curves for headloss and Pressure at Standard Conditions 101.354 14.70 psia kPa oxygen transfer capacity under standard conditions **Temperature at Standard Conditions** 68 20.0 C for ASCE testing. All conversions applied within Saturated Vapor Pressure at Standard Temperature 0.3391 psia 2.338 kPa the model for determining the effectiveness in Relative Humidity at Standard Conditions 36% specific process fluids, as compared to clean water testing, are intended as a projection of the actual Density of Air at Standard Conditions 0.075 1.201 lbs/ft^3 kg/m3 conditions expected. Tideflex Technologies shall Density of Air Correction factor 0.7378 not be responsible for the accuracy of these Corrected Density of Air at Site Elevation & Temp 0.0553 lbs/ft^3 0.886 kg/m3 projected conditions. Input Parameters for Post Aeration Systems 0.00

0.00

0.00

Required Effluent Dissolved Oxygen Concentration

RECTANGULAR TANK DIMENSIONS US UNITS Aeration Aeration Aeration Water V-Bottom Liquid Surface **V-Bottom** Dimensional Percentage Length Width Depth Depth Area Volume Volume of AOR Tank Volume feet feet cubic feet cubic feet Distrib. feet feet sq. ft. gallons AD-01 54.75 52.00 10.50 0.00 2,847 0.00 29,894 223,603 33% AD-02 29,894 54.75 52.00 10.50 0.00 2,847 0.00 223,603 33% AD-03 54.75 52.00 10.50 0.00 2,847 0.00 29,894 223,603 33%

8,541	89,681	670,810	100%
sq.ft.	cuft	gallons	

					SI UNITS				
					Aeration		Aeration	Aeration	
			Water	V-Bottom	Surface	V-Bottom	Dimensional	Liquid	Percentage
Tank	Length	Width	Depth	Depth	Area	Volume	Volume	Volume	of AOR
	meters	meters	meters	meters	sq. meters	meter^3	cubic meters	liters	Distrib.
AD-01	16.69	15.85	3.20	0.00	264	0.00	846	846,339	33%
AD-02	16.69	15.85	3.20	0.00	264	0.00	846	846,339	33%
AD-03	16.69	15.85	3.20	0.00	264	0.00	846	846,339	33%

793	2,539	2,539,016	100%
sq.m.	cu.m	L	



* (Maximum Value of AOR1, AOR2, AOR3, AOR4, AOR5 & AOR6)

COARSE BUBBLE DIFFUSER SYSTEM Number of Coarse Bubble Diffusers and Total Airflow Required

AOR = Actual Oxygen Transferred into wastewater solution

SOTR = Oxygen transfer rate based on clean water

										TFA-3.00	
	AOF	R / SOTR Ratio	20.0%								Coarse
							Airflow per	Airflow per	Efficiency	Total	Bubble
Tank	AOR	AOR	SOTR	SOTR	Airflow	Airflow	Diffuser	Diffuser	per foot	Diffuser	Diffusers
No.	kg/hr	lbs/hr	kg/hr	lbs/hr	Nm3/hr	scfm	scfm	Nm3/hr	depth	Efficiency	Required
AD-01	10.04	22.14	50.18	110.63	2,149.81	1,265.19	10.5	17.915	0.825%	8.46%	120.0
AD-02	10.04	22.14	50.18	110.63	2,149.81	1,265.19	10.5	17.915	0.825%	8.46%	120.0
AD-03	10.04	22.14	50.18	110.63	2,149.81	1,265.19	10.5	17.915	0.825%	8.46%	120.0

30.13	66.43	150.54	331.88	6,449.42	3,795.56	360
kg/hr	lbs/hr	kg/hr	lbs/hr	Nm3/hr	scfm	units

1.8% Solids - O2 & Mixing

Diffuser Model

MLSS Concentration for Activated Sludge Process = 0 mg/l Sludge Process Solids Concentration = 1.80 % Solids

Tideflex Technologies A Division of Red Valve Company, Inc.



*Note: Headloss associated to top side, field routed air supply piping, valves and blower fittings must be added to determine total system operating pressure and ICFM rate at blower.

COARSE BUBBLE DIFFUSER SYSTEM Airflow Required for Complete Mixing based on Cubic Liquid Volume of Tank

	Recommended Design Values for Mixing	Specific Weight = 62.4 lb/ft^3	
Velocity	Airflow per Volume Ratio	Dynamic	Dynamic Viscosity = 2.75E-05 lbf-s/ft^2
Gradient	cfm per 1000 cuft liquid	Viscosity	
G (sec-1)		lbf-s/ft^2	Water Level Surge
			Off Gas Rise Rate = 2.00 ft/sec
130-140	15 cfm/1000 cuft for Equalization Tank	1.22E-05	Volume of Air in Liquid = 146.49 cuft
130-140	20 cfm/1000 cuft for Aeration Tank to 2500 mg/l MLSS	1.45E-05	Liquid Level Increase = 0.62 inches
130-140	25 cfm/1000 cuft for Aeration Tank to 4500 mg/I MLSS	1.65E-05	
130-140	28 cfm/1000 cuft for Aeration Tank to 6500 mg/l MLSS	1.74E-05	MLSS Concentration = 0 mg/l
130-140	30 cfm/1000 cuft for Aerobic Sludge to 1% solids	1.95E-05	Solids Concentration = 1.8 % Solids
130-140	35 cfm/1000 cuft for Aerobic Sludge to 2% solids	2.75E-05	
130-140	40 cfm/1000 cuft for Aerobic Sludge to 3% solids	3.50E-05	
130-140	45 cfm/1000 cuft for Aerobic Sludge to 4% solids	Diffuser Model	

Step 1 - Mixing based on Volume Volume Volume		Design Unit Air Flowrate		Airflow Rate Required		Air Flowrate per Diffuser		Coarse Bubble Diffusers	
Tank	cu.ft.	cu.m.	cfm/1000 cuft	m3/hr/m3	cfm	m3/hr	cfm	m3/hr	Required
AD-01	29,894	846	57.37	3.442	1,715.00	2913.78	14.29	24.282	120.0
AD-02	29,894	846	57.37	3.442	1,715.00	2913.78	14.29	24.282	120.0
AD-03	29,894	846	57.37	3.442	1,715.00	2913.78	14.29	24.282	120.0

	89,680.50 cu.ft.	2539.4 cu.m.			5,145.00 cfm	8,741.33 m3/hr		360 units
Step 2 - V	Velocity Gradie	nt at Airflow			Equiv	valent	Mean-Squared	
	Volume	Volume	Depth	Depth	Ρον	ver	Velocity Gradient	
Tank	cu.ft.	cu.m.	feet	meters	ft-lb/sec	kW	G, sec-1	
AD-01	29,894	846	11	3	16,326	22.13	141	
AD-02	29,894	846	11	3	16,326	22.13	141	
AD-03	29,894	846	11	3	16,326	22.13	141	

TFA-030-007-6DCP40

COARSE BUBBLE AIR DIFFUSER



TIDEFLEX COARSE BUBBLE DIFFUSER

HEADLOSS VS. AIR FLOW

TFA-3.00" US UNITS



TIDEFLEX COARSE BUBBLE DIFFUSER

1.100

TFA-3.0" SOTE VS. AIR FLOW **US UNITS**

